

# Important Psychrometry Formulas PDF



Formulas  
Examples  
with Units

List of 86  
Important Psychrometry Formulas

## 1) By-Pass Factor Formulas ↗

### 1.1) By-Pass Factor of Cooling Coil Formula ↗

Formula

$$BPF = \exp\left(-\frac{U \cdot A_c}{m_{air} \cdot c}\right)$$

Example with Units

$$0.8803 = \exp\left(-\frac{50 \text{ W/m}^2\text{K} \cdot 64 \text{ m}^2}{6 \text{ kg} \cdot 4.184 \text{ kJ/kg*K}}\right)$$

Evaluate Formula ↗

### 1.2) By-Pass Factor of Heating Coil Formula ↗

Formula

$$BPF = \exp\left(-\frac{U \cdot A_c}{m_{air} \cdot c}\right)$$

Example with Units

$$0.8803 = \exp\left(-\frac{50 \text{ W/m}^2\text{K} \cdot 64 \text{ m}^2}{6 \text{ kg} \cdot 4.184 \text{ kJ/kg*K}}\right)$$

Evaluate Formula ↗

### 1.3) Efficiency of Cooling Coil Formula ↗

Formula

$$\eta = \frac{T_i - T_f}{T_i - T_c}$$

Example with Units

$$16 = \frac{105 \text{ K} - 345 \text{ K}}{105 \text{ K} - 120 \text{ K}}$$

Evaluate Formula ↗

### 1.4) Efficiency of Cooling Coil given By-pass Factor Formula ↗

Formula

$$\eta = 1 - BPF$$

Example

$$0.15 = 1 - 0.85$$

Evaluate Formula ↗

### 1.5) Efficiency of Heating Coil Formula ↗

Formula

$$\eta = \frac{T_f - T_i}{T_c - T_i}$$

Example with Units

$$16 = \frac{345 \text{ K} - 105 \text{ K}}{120 \text{ K} - 105 \text{ K}}$$

Evaluate Formula ↗

### 1.6) Efficiency of Heating Coil given By-pass Factor Formula ↗

Formula

$$\eta = 1 - BPF$$

Example

$$0.15 = 1 - 0.85$$

Evaluate Formula ↗



## 1.7) LMTD of Coil given By-Pass Factor Formula

Formula

$$\Delta T_m = \frac{T_f - T_i}{\ln\left(\frac{1}{BPF}\right)}$$

Example with Units

$$1476.7511 = \frac{345\text{K} - 105\text{K}}{\ln\left(\frac{1}{0.85}\right)}$$

Evaluate Formula 

## 1.8) Mass of Air Passing over Coil given By-Pass Factor Formula

Formula

$$m_{air} = - \left( \frac{U \cdot A_c}{c \cdot \ln(BPF)} \right)$$

Example with Units

$$4.706\text{kg} = - \left( \frac{50\text{W/m}^2\text{K} \cdot 64\text{m}^2}{4.184\text{kJ/kg}\text{K} \cdot \ln(0.85)} \right)$$

Evaluate Formula 

## 1.9) Overall Heat Transfer Coefficient given By-Pass Factor Formula

Formula

$$U = - \frac{\ln(BPF) \cdot m_{air} \cdot c}{A_c}$$

Example with Units

$$63.7481\text{W/m}^2\text{K} = - \frac{\ln(0.85) \cdot 6\text{kg} \cdot 4.184\text{kJ/kg}\text{K}}{64\text{m}^2}$$

Evaluate Formula 

## 1.10) Sensible Heat given Out by Coil using By-Pass Factor Formula

Formula

$$SH = \frac{U \cdot A_c \cdot (T_f - T_i)}{\ln\left(\frac{1}{BPF}\right)}$$

Example with Units

$$4.7E+6\text{J} = \frac{50\text{W/m}^2\text{K} \cdot 64\text{m}^2 \cdot (345\text{K} - 105\text{K})}{\ln\left(\frac{1}{0.85}\right)}$$

Evaluate Formula 

## 1.11) Surface Area of Coil given By-Pass Factor Formula

Formula

$$A_c = - \frac{\ln(BPF) \cdot m_{air} \cdot c}{U}$$

Example with Units

$$81.5975\text{m}^2 = - \frac{\ln(0.85) \cdot 6\text{kg} \cdot 4.184\text{kJ/kg}\text{K}}{50\text{W/m}^2\text{K}}$$

Evaluate Formula 

## 1.12) Wet Bulb Depression Formula

Formula

$$WBD = t_{db} - T_w$$

Example

$$96 = 110 - 14$$

Evaluate Formula 

## 2) Degree of Saturation Formulas

### 2.1) Degree of Saturation given Partial Pressure of Water Vapour Formula

Formula

$$S = \frac{p_v}{p_s} \cdot \frac{1 - \frac{p_s}{p_t}}{1 - \frac{p_v}{p_t}}$$

Example with Units

$$0.1484 = \frac{60\text{Bar}}{91\text{Bar}} \cdot \frac{1 - \frac{91\text{Bar}}{100\text{Bar}}}{1 - \frac{60\text{Bar}}{100\text{Bar}}}$$

Evaluate Formula 



## 2.2) Degree of Saturation given Relative Humidity Formula ↗

**Formula**

$$S = \Phi \cdot \frac{1 - \frac{p_s}{p_t}}{1 - \frac{\Phi \cdot p_s}{p_t}}$$

**Example with Units**

$$0.1264 = 0.616523 \cdot \frac{1 - \frac{91 \text{ Bar}}{100 \text{ Bar}}}{1 - \frac{0.616523 \cdot 91 \text{ Bar}}{100 \text{ Bar}}}$$

Evaluate Formula ↗

## 2.3) Degree of Saturation given Specific Humidity Formula ↗

**Formula**

$$S = \frac{\omega}{\omega_s}$$

**Example**

$$0.2632 = \frac{0.25}{0.95}$$

Evaluate Formula ↗

## 2.4) Partial Pressure of Water Vapor in Saturated Air given Degree of Saturation Formula ↗

**Formula**

$$p_s = \left( \frac{1}{p_t} + \frac{S}{p_v} \cdot \left( 1 - \frac{p_v}{p_t} \right) \right)^{-1}$$

**Example with Units**

$$88.2353 \text{ Bar} = \left( \frac{1}{100 \text{ Bar}} + \frac{0.2}{60 \text{ Bar}} \cdot \left( 1 - \frac{60 \text{ Bar}}{100 \text{ Bar}} \right) \right)^{-1}$$

Evaluate Formula ↗

## 2.5) Total Pressure of Moist Air given Degree of Saturation Formula ↗

**Formula**

$$p_t = \frac{(S - 1) \cdot p_s \cdot p_v}{S \cdot p_s - p_v}$$

**Example with Units**

$$104.4976 \text{ Bar} = \frac{(0.2 - 1) \cdot 91 \text{ Bar} \cdot 60 \text{ Bar}}{0.2 \cdot 91 \text{ Bar} - 60 \text{ Bar}}$$

Evaluate Formula ↗

## 3) Enthalpy Formulas ↗

### 3.1) Dry Bulb Temperature given Enthalpy of Moist Air Formula ↗

**Formula**

$$t_{db} = \frac{h - 2500 \cdot \omega}{1.005 + 1.9 \cdot \omega}$$

**Example with Units**

$$1469.5946 = \frac{2800 \text{ kJ/kg} - 2500 \cdot 0.25}{1.005 + 1.9 \cdot 0.25}$$

Evaluate Formula ↗

### 3.2) Enthalpy of Dry Air Formula ↗

**Formula**

$$h_{dry} = 1.005 \cdot t_{db}$$

**Example with Units**

$$110.55 \text{ kJ/kg} = 1.005 \cdot 110$$

Evaluate Formula ↗

### 3.3) Enthalpy of Moist Air Formula ↗

**Formula**

$$h = 1.005 \cdot t_{db} + \omega \cdot (2500 + 1.9 \cdot t_{db})$$

**Example with Units**

$$787.8 \text{ kJ/kg} = 1.005 \cdot 110 + 0.25 \cdot (2500 + 1.9 \cdot 110)$$

Evaluate Formula ↗



### 3.4) Specific Enthalpy of Water Vapor Formula

[Evaluate Formula](#)**Formula****Example with Units**

$$h_{\text{dry}} = 2500 + 1.9 \cdot t_{\text{db}}$$

$$2709 \text{ kJ/kg} = 2500 + 1.9 \cdot 110$$

### 3.5) Specific Humidity given Enthalpy of Moist Air Formula

[Evaluate Formula](#)**Formula****Example with Units**

$$\omega = \frac{h - 1.005 \cdot t_{\text{db}}}{2500 + 1.9 \cdot t_{\text{db}}}$$

$$0.9928 = \frac{2800 \text{ kJ/kg} - 1.005 \cdot 110}{2500 + 1.9 \cdot 110}$$

### 3.6) Enthalpy of Saturated Air Formulas

#### 3.6.1) Coefficient of Performance given enthalpy of liquid refrigerant leaving condenser ( $h_f3$ ) Formula

[Evaluate Formula](#)**Formula****Example with Units**

$$\text{COP}_{\text{theoretical}} = \frac{h_1 - h_f3}{h_2 - h_1}$$

$$11.2 = \frac{260 \text{ kJ/kg} - 36 \text{ kJ/kg}}{280 \text{ kJ/kg} - 260 \text{ kJ/kg}}$$

#### 3.6.2) Enthalpy at point 1 given Liquid enthalpy at point 1 Formula

[Evaluate Formula](#)**Formula****Example with Units**

$$h_1 = h_{f1} + x_1 \cdot h_{fg}$$

$$200 \text{ kJ/kg} = 100 \text{ kJ/kg} + 0.1 \cdot 1000 \text{ kJ/kg}$$

#### 3.6.3) Enthalpy at point 2 Formula

[Evaluate Formula](#)**Formula****Example with Units**

$$h_2 = h_{f2} + (x_2 \cdot h_{fg})$$

$$350 \text{ kJ/kg} = 150 \text{ kJ/kg} + (0.2 \cdot 1000 \text{ kJ/kg})$$

#### 3.6.4) Enthalpy at Point 4 given Liquid Enthalpy at Point 4 Formula

[Evaluate Formula](#)**Formula****Example with Units**

$$h_4 = h_{f4} + (x_4 \cdot h_{fg})$$

$$880 \text{ kJ/kg} = 80 \text{ kJ/kg} + (0.8 \cdot 1000 \text{ kJ/kg})$$

#### 3.6.5) Entropy at point 1 Formula

[Evaluate Formula](#)**Formula****Example with Units**

$$s_1 = s_{f1} + \left( \frac{x_1 \cdot h_{fg}}{T_1} \right)$$

$$3.4 \text{ kJ/kg*K} = 3 \text{ kJ/kg*K} + \left( \frac{0.1 \cdot 1000 \text{ kJ/kg}}{250 \text{ K}} \right)$$



### 3.6.6) Entropy at point 2 Formula

**Formula**

$$s_2 = s_{f2} + \left( \frac{x_2 \cdot h_{fg}}{T_2} \right)$$

**Example with Units**

$$7.4444 \text{ kJ/kg*K} = 7 \text{ kJ/kg} + \left( \frac{0.2 \cdot 1000 \text{ kJ/kg}}{450 \text{ K}} \right)$$

**Evaluate Formula**

### 3.6.7) Refrigerating Effect given Enthalpy at Inlet of Compressor and Exit of Condenser Formula

**Formula**

$$R_E = h_1 - h_{f3}$$

**Example with Units**

$$224 \text{ kJ/kg} = 260 \text{ kJ/kg} - 36 \text{ kJ/kg}$$

**Evaluate Formula**

### 3.6.8) Refrigerating Effect(for given h1 and h4) Formula

**Formula**

$$R_E = h_1 - h_4$$

**Example with Units**

$$80 \text{ kJ/kg} = 260 \text{ kJ/kg} - 180 \text{ kJ/kg}$$

**Evaluate Formula**

### 3.6.9) Work done during isentropic compression(per Kg of refrigerant) Formula

**Formula**

$$w = h_2 - h_1$$

**Example with Units**

$$20 \text{ kJ} = 280 \text{ kJ/kg} - 260 \text{ kJ/kg}$$

**Evaluate Formula**

### 3.6.10) Theoretical Vapour compression cycle with Wet vapour after compression Formulas

#### 3.6.10.1) Coefficient of Performance given enthalpy of liquid refrigerant leaving condenser (hf3) Formula

**Formula**

$$\text{COP}_{\text{theoretical}} = \frac{h_1 - h_{f3}}{h_2 - h_1}$$

**Example with Units**

$$11.2 = \frac{260 \text{ kJ/kg} - 36 \text{ kJ/kg}}{280 \text{ kJ/kg} - 260 \text{ kJ/kg}}$$

**Evaluate Formula**

#### 3.6.10.2) Enthalpy at point 1 given Liquid enthalpy at point 1 Formula

**Formula**

$$h_1 = h_{f1} + x_1 \cdot h_{fg}$$

**Example with Units**

$$200 \text{ kJ/kg} = 100 \text{ kJ/kg} + 0.1 \cdot 1000 \text{ kJ/kg}$$

**Evaluate Formula**

#### 3.6.10.3) Enthalpy at point 2 Formula

**Formula**

$$h_2 = h_{f2} + (x_2 \cdot h_{fg})$$

**Example with Units**

$$350 \text{ kJ/kg} = 150 \text{ kJ/kg} + (0.2 \cdot 1000 \text{ kJ/kg})$$

**Evaluate Formula**

#### 3.6.10.4) Enthalpy at Point 4 given Liquid Enthalpy at Point 4 Formula

**Formula**

$$h_4 = h_{f4} + (x_4 \cdot h_{fg})$$

**Example with Units**

$$880 \text{ kJ/kg} = 80 \text{ kJ/kg} + (0.8 \cdot 1000 \text{ kJ/kg})$$

**Evaluate Formula**

### 3.6.10.5) Entropy at point 1 Formula

**Formula**

$$s_1 = s_{f1} + \left( \frac{x_1 \cdot h_{fg}}{T_1} \right)$$

**Example with Units**

$$3.4 \text{ kJ/kg*K} = 3 \text{ kJ/kg*K} + \left( \frac{0.1 \cdot 1000 \text{ kJ/kg}}{250 \text{ K}} \right)$$

**Evaluate Formula** 

### 3.6.10.6) Entropy at point 2 Formula

**Formula**

$$s_2 = s_{f2} + \left( \frac{x_2 \cdot h_{fg}}{T_2} \right)$$

**Example with Units**

$$7.4444 \text{ kJ/kg*K} = 7 \text{ kJ/kg*K} + \left( \frac{0.2 \cdot 1000 \text{ kJ/kg}}{450 \text{ K}} \right)$$

**Evaluate Formula** 

### 3.6.10.7) Refrigerating Effect given Enthalpy at Inlet of Compressor and Exit of Condenser Formula

**Formula**

$$R_E = h_1 - h_{f3}$$

**Example with Units**

$$224 \text{ kJ/kg} = 260 \text{ kJ/kg} - 36 \text{ kJ/kg}$$

**Evaluate Formula** 

### 3.6.10.8) Refrigerating Effect(for given h1 and h4) Formula

**Formula**

$$R_E = h_1 - h_4$$

**Example with Units**

$$80 \text{ kJ/kg} = 260 \text{ kJ/kg} - 180 \text{ kJ/kg}$$

**Evaluate Formula** 

### 3.6.11) Theoretical Vapour compression cycle with Superheated vapour after compression Formulas

#### 3.6.11.1) Coefficient of Performance given enthalpy of liquid refrigerant leaving condenser (hf3) Formula

**Formula**

$$\text{COP}_{\text{theoretical}} = \frac{h_1 - h_{f3}}{h_2 - h_1}$$

**Example with Units**

$$11.2 = \frac{260 \text{ kJ/kg} - 36 \text{ kJ/kg}}{280 \text{ kJ/kg} - 260 \text{ kJ/kg}}$$

**Evaluate Formula** 

#### 3.6.11.2) Enthalpy at point 1 given Liquid enthalpy at point 1 Formula

**Formula**

$$h_1 = h_{f1} + x_1 \cdot h_{fg}$$

**Example with Units**

$$200 \text{ kJ/kg} = 100 \text{ kJ/kg} + 0.1 \cdot 1000 \text{ kJ/kg}$$

**Evaluate Formula** 

#### 3.6.11.3) Enthalpy at point 2 Formula

**Formula**

$$h_2 = h_{f2} + (x_2 \cdot h_{fg})$$

**Example with Units**

$$350 \text{ kJ/kg} = 150 \text{ kJ/kg} + (0.2 \cdot 1000 \text{ kJ/kg})$$

**Evaluate Formula** 

### 3.6.11.4) Enthalpy at Point 4 given Liquid Enthalpy at Point 4 Formula

Formula

$$h_4 = h_{f4} + (x_4 \cdot h_{fg})$$

Example with Units

$$880 \text{ kJ/kg} = 80 \text{ kJ/kg} + (0.8 \cdot 1000 \text{ kJ/kg})$$

Evaluate Formula

### 3.6.11.5) Entropy at point 1 Formula

Formula

$$s_1 = s_{f1} + \left( \frac{x_1 \cdot h_{fg}}{T_1} \right)$$

Example with Units

$$3.4 \text{ kJ/kg*K} = 3 \text{ kJ/kg*K} + \left( \frac{0.1 \cdot 1000 \text{ kJ/kg}}{250 \text{ K}} \right)$$

Evaluate Formula

### 3.6.11.6) Entropy at point 2 Formula

Formula

$$s_2 = s_{f2} + \left( \frac{x_2 \cdot h_{fg}}{T_2} \right)$$

Example with Units

$$7.4444 \text{ kJ/kg*K} = 7 \text{ kJ/kg*K} + \left( \frac{0.2 \cdot 1000 \text{ kJ/kg}}{450 \text{ K}} \right)$$

Evaluate Formula

### 3.6.11.7) Refrigerating Effect given Enthalpy at Inlet of Compressor and Exit of Condenser Formula

Formula

$$R_E = h_1 - h_3$$

Example with Units

$$224 \text{ kJ/kg} = 260 \text{ kJ/kg} - 36 \text{ kJ/kg}$$

Evaluate Formula

### 3.6.11.8) Refrigerating Effect(for given h1 and h4) Formula

Formula

$$R_E = h_1 - h_4$$

Example with Units

$$80 \text{ kJ/kg} = 260 \text{ kJ/kg} - 180 \text{ kJ/kg}$$

Evaluate Formula

### 3.6.12) Theoretical Vapour compression cycle with Superheated vapour before compression Formulas

#### 3.6.12.1) Coefficient of Performance given enthalpy of liquid refrigerant leaving condenser (hf3) Formula

Formula

$$\text{COP}_{\text{theoretical}} = \frac{h_1 - h_3}{h_2 - h_1}$$

Example with Units

$$11.2 = \frac{260 \text{ kJ/kg} - 36 \text{ kJ/kg}}{280 \text{ kJ/kg} - 260 \text{ kJ/kg}}$$

Evaluate Formula

#### 3.6.12.2) Enthalpy at point 1 given Liquid enthalpy at point 1 Formula

Formula

$$h_1 = h_{f1} + x_1 \cdot h_{fg}$$

Example with Units

$$200 \text{ kJ/kg} = 100 \text{ kJ/kg} + 0.1 \cdot 1000 \text{ kJ/kg}$$

Evaluate Formula



### 3.6.12.3) Enthalpy at point 2 Formula

**Formula**

$$h_2 = h_{f2} + (x_2 \cdot h_{fg})$$

**Example with Units**

$$350 \text{ kJ/kg} = 150 \text{ kJ/kg} + (0.2 \cdot 1000 \text{ kJ/kg})$$

**Evaluate Formula** 

### 3.6.12.4) Enthalpy at Point 4 given Liquid Enthalpy at Point 4 Formula

**Formula**

$$h_4 = h_{f4} + (x_4 \cdot h_{fg})$$

**Example with Units**

$$880 \text{ kJ/kg} = 80 \text{ kJ/kg} + (0.8 \cdot 1000 \text{ kJ/kg})$$

**Evaluate Formula** 

### 3.6.12.5) Entropy at point 1 Formula

**Formula**

$$s_1 = s_{f1} + \left( \frac{x_1 \cdot h_{fg}}{T_1} \right)$$

**Example with Units**

$$3.4 \text{ kJ/kg*K} = 3 \text{ kJ/kg*K} + \left( \frac{0.1 \cdot 1000 \text{ kJ/kg}}{250 \text{ K}} \right)$$

**Evaluate Formula** 

### 3.6.12.6) Entropy at point 2 Formula

**Formula**

$$s_2 = s_{f2} + \left( \frac{x_2 \cdot h_{fg}}{T_2} \right)$$

**Example with Units**

$$7.4444 \text{ kJ/kg*K} = 7 \text{ kJ/kg*K} + \left( \frac{0.2 \cdot 1000 \text{ kJ/kg}}{450 \text{ K}} \right)$$

**Evaluate Formula** 

### 3.6.12.7) Refrigerating Effect given Enthalpy at Inlet of Compressor and Exit of Condenser Formula

**Formula**

$$R_E = h_1 - h_{f3}$$

**Example with Units**

$$224 \text{ kJ/kg} = 260 \text{ kJ/kg} - 36 \text{ kJ/kg}$$

**Evaluate Formula** 

### 3.6.12.8) Refrigerating Effect(for given h1 and h4) Formula

**Formula**

$$R_E = h_1 - h_4$$

**Example with Units**

$$80 \text{ kJ/kg} = 260 \text{ kJ/kg} - 180 \text{ kJ/kg}$$

**Evaluate Formula** 

### 3.6.13) Theoretical Vapour compression cycle with Under-cooling or sub-cooling if refrigerant Formulas

#### 3.6.13.1) Coefficient of Performance given enthalpy of liquid refrigerant leaving condenser ( $h_{f3}$ ) Formula

**Formula**

$$\text{COP}_{\text{theoretical}} = \frac{h_1 - h_{f3}}{h_2 - h_1}$$

**Example with Units**

$$11.2 = \frac{260 \text{ kJ/kg} - 36 \text{ kJ/kg}}{280 \text{ kJ/kg} - 260 \text{ kJ/kg}}$$

**Evaluate Formula** 

### 3.6.13.2) Enthalpy at point 1 given Liquid enthalpy at point 1 Formula

**Formula**

$$h_1 = h_{f1} + x_1 \cdot h_{fg}$$

**Example with Units**

$$200 \text{ kJ/kg} = 100 \text{ kJ/kg} + 0.1 \cdot 1000 \text{ kJ/kg}$$

**Evaluate Formula** 

### 3.6.13.3) Enthalpy at point 2 Formula

**Formula**

$$h_2 = h_{f2} + (x_2 \cdot h_{fg})$$

**Example with Units**

$$350 \text{ kJ/kg} = 150 \text{ kJ/kg} + (0.2 \cdot 1000 \text{ kJ/kg})$$

**Evaluate Formula** 

### 3.6.13.4) Enthalpy at Point 4 given Liquid Enthalpy at Point 4 Formula

**Formula**

$$h_4 = h_{f4} + (x_4 \cdot h_{fg})$$

**Example with Units**

$$880 \text{ kJ/kg} = 80 \text{ kJ/kg} + (0.8 \cdot 1000 \text{ kJ/kg})$$

**Evaluate Formula** 

### 3.6.13.5) Entropy at point 1 Formula

**Formula**

$$s_1 = s_{f1} + \left( \frac{x_1 \cdot h_{fg}}{T_1} \right)$$

**Example with Units**

$$3.4 \text{ kJ/kg*K} = 3 \text{ kJ/kg*K} + \left( \frac{0.1 \cdot 1000 \text{ kJ/kg}}{250 \text{ K}} \right)$$

**Evaluate Formula** 

### 3.6.13.6) Entropy at point 2 Formula

**Formula**

$$s_2 = s_{f2} + \left( \frac{x_2 \cdot h_{fg}}{T_2} \right)$$

**Example with Units**

$$7.4444 \text{ kJ/kg*K} = 7 \text{ kJ/kg*K} + \left( \frac{0.2 \cdot 1000 \text{ kJ/kg}}{450 \text{ K}} \right)$$

**Evaluate Formula** 

### 3.6.13.7) Refrigerating Effect given Enthalpy at Inlet of Compressor and Exit of Condenser Formula

**Formula**

$$R_E = h_1 - h_{f3}$$

**Example with Units**

$$224 \text{ kJ/kg} = 260 \text{ kJ/kg} - 36 \text{ kJ/kg}$$

**Evaluate Formula** 

### 3.6.13.8) Refrigerating Effect(for given h1 and h4) Formula

**Formula**

$$R_E = h_1 - h_4$$

**Example with Units**

$$80 \text{ kJ/kg} = 260 \text{ kJ/kg} - 180 \text{ kJ/kg}$$

**Evaluate Formula** 

## 4) Enthalpy of Moist air Formulas

## 5) Humidity Formulas



## 5.1) Relative Humidity Formulas

### 5.1.1) Partial Pressure of Vapor given Relative Humidity Formula

Formula

$$p_v = \Phi \cdot p_s$$

Example with Units

$$56.1036 \text{ Bar} = 0.616523 \cdot 91 \text{ Bar}$$

Evaluate Formula 

### 5.1.2) Relative Humidity given Degree of Saturation Formula

Formula

$$\Phi = \frac{s}{1 - \frac{p_s}{p_t} \cdot (1 - s)}$$

Example with Units

$$0.7353 = \frac{0.2}{1 - \frac{91 \text{ Bar}}{100 \text{ Bar}} \cdot (1 - 0.2)}$$

Evaluate Formula 

### 5.1.3) Relative Humidity given Mass of Water Vapor Formula

Formula

$$\Phi = \frac{m_v}{m_s}$$

Example with Units

$$0.6 = \frac{3 \text{ kg}}{5 \text{ kg}}$$

Evaluate Formula 

### 5.1.4) Relative Humidity given Partial Pressure of Water Vapor Formula

Formula

$$\Phi = \frac{p_v}{p_s}$$

Example with Units

$$0.6593 = \frac{60 \text{ Bar}}{91 \text{ Bar}}$$

Evaluate Formula 

### 5.1.5) Saturation Pressure of Water Vapor given Relative Humidity Formula

Formula

$$p_s = \frac{p_v}{\Phi}$$

Example with Units

$$97.32 \text{ Bar} = \frac{60 \text{ Bar}}{0.616523}$$

Evaluate Formula 

## 5.2) Specific Humidity Formulas

### 5.2.1) Maximum Specific Humidity Formula

Formula

$$\omega_{\max} = \frac{0.622 \cdot p_s}{p_t - p_s}$$

Example with Units

$$6.2891 = \frac{0.622 \cdot 91 \text{ Bar}}{100 \text{ Bar} - 91 \text{ Bar}}$$

Evaluate Formula 

### 5.2.2) Partial Pressure of Dry Air given Specific Humidity Formula

Formula

$$p_a = \frac{0.622 \cdot p_v}{\omega}$$

Example with Units

$$149.28 \text{ Bar} = \frac{0.622 \cdot 60 \text{ Bar}}{0.25}$$

Evaluate Formula 



### 5.2.3) Partial Pressure of Water Vapor given Specific Humidity Formula

**Formula**

$$p_v = \frac{p_t}{1 + \frac{0.622}{\omega}}$$

**Example with Units**

$$28.6697 \text{ Bar} = \frac{100 \text{ Bar}}{1 + \frac{0.622}{0.25}}$$

**Evaluate Formula** 

### 5.2.4) Specific Humidity given Mass of Water Vapor and Dry Air Formula

**Formula**

$$\omega = \frac{m_v}{m_a}$$

**Example with Units**

$$0.3 = \frac{3 \text{ kg}}{10 \text{ kg}}$$

**Evaluate Formula** 

### 5.2.5) Specific Humidity given Partial Pressure of Water Vapor Formula

**Formula**

$$\omega = \frac{0.622 \cdot p_v}{p_t - p_v}$$

**Example with Units**

$$0.933 = \frac{0.622 \cdot 60 \text{ Bar}}{100 \text{ Bar} - 60 \text{ Bar}}$$

**Evaluate Formula** 

### 5.2.6) Specific Humidity given Specific Volumes Formula

**Formula**

$$\omega = \frac{v_a}{v_v}$$

**Example with Units**

$$0.4 = \frac{0.02 \text{ m}^3/\text{kg}}{0.05 \text{ m}^3/\text{kg}}$$

**Evaluate Formula** 

### 5.2.7) Total Pressure of Moist Air given Specific Humidity Formula

**Formula**

$$p_t = p_v + \frac{0.622 \cdot p_v}{\omega}$$

**Example with Units**

$$209.28 \text{ Bar} = 60 \text{ Bar} + \frac{0.622 \cdot 60 \text{ Bar}}{0.25}$$

**Evaluate Formula** 

## 6) Pressure of Water Vapor Formulas

### 6.1) Dry Bulb Temperature using Carrier's Equation Formula

**Formula**

$$t_{db} = \left( \left( p_w - p_v \right) \cdot \frac{1544 - 1.44 \cdot T_w}{p_t - p_w} \right) + T_w$$

**Evaluate Formula** **Example with Units**

$$231.6914 = \left( \left( 65 \text{ Bar} - 60 \text{ Bar} \right) \cdot \frac{1544 - 1.44 \cdot 14}{100 \text{ Bar} - 65 \text{ Bar}} \right) + 14$$

## 6.2) Partial Pressure of Water Vapor Formula [🔗](#)

[Evaluate Formula \[🔗\]\(#\)](#)

Formula

$$p_v = p_w - \frac{(p_t - p_w) \cdot (t_{db} - T_w)}{1544 - 1.44 \cdot T_w}$$

Example with Units

$$62.795 \text{ Bar} = 65 \text{ Bar} - \frac{(100 \text{ Bar} - 65 \text{ Bar}) \cdot (110 - 14)}{1544 - 1.44 \cdot 14}$$

## 6.3) Saturation Pressure Corresponding to Wet Bulb Temperature Formula [🔗](#)

[Evaluate Formula \[🔗\]\(#\)](#)

Formula

Example with Units

$$p_w = \frac{p_v + p_t \cdot \left( \frac{t_{db} - T_w}{1544 - 1.44 \cdot T_w} \right)}{1 + \left( \frac{t_{db} - T_w}{1544 - 1.44 \cdot T_w} \right)}$$

$$62.3706 \text{ Bar} = \frac{60 \text{ Bar} + 100 \text{ Bar} \cdot \left( \frac{110 - 14}{1544 - 1.44 \cdot 14} \right)}{1 + \left( \frac{110 - 14}{1544 - 1.44 \cdot 14} \right)}$$

## 6.4) Total Pressure of Moist Air using Carrier's Equation Formula [🔗](#)

[Evaluate Formula \[🔗\]\(#\)](#)

Formula

$$p_t = \frac{(p_w - p_v) \cdot (1544 - 1.44 \cdot T_w)}{t_{db} - T_w} + p_w$$

Example with Units

$$144.3667 \text{ Bar} = \frac{(65 \text{ Bar} - 60 \text{ Bar}) \cdot (1544 - 1.44 \cdot 14)}{110 - 14} + 65 \text{ Bar}$$

## 6.5) Wet Bulb Temperature using Carrier's Equation Formula [🔗](#)

[Evaluate Formula \[🔗\]\(#\)](#)

Formula

$$T_w = \frac{1544 \cdot (p_w - p_v) - t_{db} \cdot (p_t - p_w)}{1.44 \cdot (p_w - p_v) - (p_t - p_w)}$$

Example with Units

$$-139.2086 = \frac{1544 \cdot (65 \text{ Bar} - 60 \text{ Bar}) - 110 \cdot (100 \text{ Bar} - 65 \text{ Bar})}{1.44 \cdot (65 \text{ Bar} - 60 \text{ Bar}) - (100 \text{ Bar} - 65 \text{ Bar})}$$

## 7) Relative Humidity Formulas [🔗](#)

## 8) Specific Humidity Formulas [🔗](#)



## 9) Vapour Density Formulas ↗

### 9.1) Dry Bulb Temperature given Vapor Density Formula ↗

**Formula**

$$t_d = \frac{\omega \cdot (p_t - p_v)}{287 \cdot \rho_v}$$

**Example with Units**

$$108.885 \text{ K} = \frac{0.25 \cdot (100 \text{ Bar} - 60 \text{ Bar})}{287 \cdot 32 \text{ kg/m}^3}$$

**Evaluate Formula ↗**

### 9.2) Partial Pressure of Dry Air given Vapor Density Formula ↗

**Formula**

$$p_a = \frac{\rho_v \cdot 287 \cdot t_d}{\omega}$$

**Example with Units**

$$128.576 \text{ Bar} = \frac{32 \text{ kg/m}^3 \cdot 287 \cdot 350 \text{ K}}{0.25}$$

**Evaluate Formula ↗**

### 9.3) Partial Pressure of Vapor given Vapor Density Formula ↗

**Formula**

$$p_v = p_t - \left( \frac{\rho_v \cdot 287 \cdot t_d}{\omega} \right)$$

**Example with Units**

$$-28.576 \text{ Bar} = 100 \text{ Bar} - \left( \frac{32 \text{ kg/m}^3 \cdot 287 \cdot 350 \text{ K}}{0.25} \right)$$

**Evaluate Formula ↗**

### 9.4) Specific Humidity given Vapor Density Formula ↗

**Formula**

$$\omega = \frac{\rho_v \cdot t_d \cdot 287}{p_t - p_v}$$

**Example with Units**

$$0.8036 = \frac{32 \text{ kg/m}^3 \cdot 350 \text{ K} \cdot 287}{100 \text{ Bar} - 60 \text{ Bar}}$$

**Evaluate Formula ↗**

### 9.5) Total Pressure of Moist Air given Vapour Density Formula ↗

**Formula**

$$p_t = \frac{287 \cdot \rho_v \cdot t_d}{\omega} + p_v$$

**Example with Units**

$$188.576 \text{ Bar} = \frac{287 \cdot 32 \text{ kg/m}^3 \cdot 350 \text{ K}}{0.25} + 60 \text{ Bar}$$

**Evaluate Formula ↗**

### 9.6) Vapour Density Formula ↗

**Formula**

$$\rho_v = \frac{\omega \cdot (p_t - p_v)}{287 \cdot t_d}$$

**Example with Units**

$$9.9552 \text{ kg/m}^3 = \frac{0.25 \cdot (100 \text{ Bar} - 60 \text{ Bar})}{287 \cdot 350 \text{ K}}$$

**Evaluate Formula ↗**

## Variables used in list of Psychrometry Formulas above

- $A_c$  Surface Area of Coil (Square Meter)
- $BPF$  By Pass Factor
- $c$  Specific Heat Capacity (Kilojoule per Kilogram per K)
- $COP_{theoretical}$  Theoretical Coefficient of Performance
- $h$  Enthalpy of Moist Air (Kilojoule per Kilogram)
- $h_1$  Enthalpy of the Vapour Refrigerant at T1 (Kilojoule per Kilogram)
- $h_2$  Enthalpy of the vapour refrigerant at T2 (Kilojoule per Kilogram)
- $h_4$  Enthalpy of the vapour refrigerant at T4 (Kilojoule per Kilogram)
- $h_{dry}$  Enthalpy of Dry Air (Kilojoule per Kilogram)
- $h_{f1}$  Liquid Enthalpy at Point 1 (Kilojoule per Kilogram)
- $h_{f2}$  Liquid Enthalpy at Point 2 (Kilojoule per Kilogram)
- $h_{f4}$  Liquid Enthalpy at Point 4 (Kilojoule per Kilogram)
- $h_{fg}$  Latent Heat of Fusion (Kilojoule per Kilogram)
- $h_{f3}$  Sensible Heat at Temperature T3 (Kilojoule per Kilogram)
- $m_a$  Mass of Dry Air (Kilogram)
- $m_{air}$  Mass of Air (Kilogram)
- $m_s$  Mass of Water Vapor in Saturated Air (Kilogram)
- $m_v$  Mass of Water Vapor in Moist Air (Kilogram)
- $p_a$  Partial Pressure of Dry Air (Bar)
- $p_s$  Partial Pressure of Water Vapour in Saturated Air (Bar)
- $p_t$  Total Pressure of Moist Air (Bar)
- $p_v$  Pressure of Water Vapor (Bar)
- $p_w$  Saturation Pressure Corresponding to WBT (Bar)

## Constants, Functions, Measurements used in list of Psychrometry Formulas above

- **Functions:**  $\exp$ ,  $\exp(\text{Number})$   
*n an exponential function, the value of the function changes by a constant factor for every unit change in the independent variable.*
- **Functions:**  $\ln$ ,  $\ln(\text{Number})$   
*The natural logarithm, also known as the logarithm to the base e, is the inverse function of the natural exponential function.*
- **Measurement:** **Weight** in Kilogram (kg)  
*Weight Unit Conversion*
- **Measurement:** **Temperature** in Kelvin (K)  
*Temperature Unit Conversion*
- **Measurement:** **Area** in Square Meter ( $\text{m}^2$ )  
*Area Unit Conversion*
- **Measurement:** **Pressure** in Bar (Bar)  
*Pressure Unit Conversion*
- **Measurement:** **Energy** in Joule (J), Kilojoule (kJ)  
*Energy Unit Conversion*
- **Measurement:** **Heat of Combustion (per Mass)** in Kilojoule per Kilogram (kJ/kg)  
*Heat of Combustion (per Mass) Unit Conversion*
- **Measurement:** **Specific Heat Capacity** in Kilojoule per Kilogram per K (kJ/kg\*K)  
*Specific Heat Capacity Unit Conversion*
- **Measurement:** **Heat Transfer Coefficient** in Watt per Square Meter per Kelvin (W/m<sup>2</sup>\*K)  
*Heat Transfer Coefficient Unit Conversion*
- **Measurement:** **Density** in Kilogram per Cubic Meter (kg/m<sup>3</sup>)  
*Density Unit Conversion*
- **Measurement:** **Specific Volume** in Cubic Meter per Kilogram (m<sup>3</sup>/kg)  
*Specific Volume Unit Conversion*
- **Measurement:** **Specific Entropy** in Kilojoule per Kilogram K (kJ/kg\*K)  
*Specific Entropy Unit Conversion*



- **R<sub>E</sub>** Refrigerating Effect (*Kilojoule per Kilogram*)
- **S** Degree of Saturation
- **S<sub>1</sub>** Entropy at Point 1 (*Kilojoule per Kilogram K*)
- **S<sub>2</sub>** Entropy at point 2 (*Kilojoule per Kilogram K*)
- **S<sub>f1</sub>** Liquid Entropy at Point 1 (*Kilojoule per Kilogram K*)
- **S<sub>f2</sub>** Liquid entropy at point 2 (*Kilojoule per Kilogram K*)
- **SH** Sensible Heat (*Joule*)
- **T<sub>1</sub>** Temperature at the suction of compressor (*Kelvin*)
- **T<sub>2</sub>** Temperature at Discharge of Compressor (*Kelvin*)
- **T<sub>c</sub>** Temperature of Coil (*Kelvin*)
- **t<sub>d</sub>** Dry Bulb Temperature (*Kelvin*)
- **t<sub>db</sub>** Dry Bulb Temperature in °C
- **T<sub>f</sub>** Final Temperature (*Kelvin*)
- **T<sub>i</sub>** Initial Temperature (*Kelvin*)
- **T<sub>w</sub>** Wet Bulb Temperature
- **U** Overall Heat Transfer Coefficient (*Watt per Square Meter per Kelvin*)
- **W** Work Done (*Kilojoule*)
- **WBD** Wet Bulb Depression
- **x<sub>1</sub>** Dryness Fraction at point 1
- **x<sub>2</sub>** Dryness Fraction at point 2
- **x<sub>4</sub>** Dryness Fraction at point 4
- **ΔT<sub>m</sub>** Logarithmic Mean Temperature Difference
- **η** Efficiency
- **v<sub>a</sub>** Specific Volume of Dry Air (*Cubic Meter per Kilogram*)
- **v<sub>v</sub>** Specific Volume of Water Vapor (*Cubic Meter per Kilogram*)
- **ρ<sub>v</sub>** Vapor Density (*Kilogram per Cubic Meter*)
- **Φ** Relative Humidity
- **ω** Specific Humidity
- **ω<sub>max</sub>** Maximum Specific Humidity

- $\omega_s$  Specific Humidity of Saturated Air

- [Important Ducts Formulas](#) ↗
- [Important Psychrometry Formulas](#) ↗

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